

**Chemistry 366  
Thermodynamics  
Midterm Exam  
March 4, 2008**



Name \_\_\_\_\_

**Full credit will be given to correct answers only when ALL the necessary steps are shown. DO NOT GUESS THE ANSWER.**

**This is a closed book exam, and you are responsible to be sure that your exam has no missing pages (5 pages).**

**If you consider that there is not enough information to solve a problem, you have to specify the missing information and describe the problem solving procedure.**

*But surely this is an old tale you tell, they say;  
But surly this is a new tale you tell, other say.  
Tell it once again, they say;  
Or, do not tell it yet again, others say.  
But I have heard all this before, say some;  
Or, but this is not how it was before, say the rest*

Naqshbandi recital, from The Way of the Sufi, by Idries Shah

**Once you start the exam, you have up to 1 hours to solve it.**

**Honor Statement**

**I have neither give nor received aid in this examination.**

**Full signature \_\_\_\_\_**

**PROBLEM 1 (25 POINTS)**

Calculate the pressure exerted by benzene for a molar volume 1.42 L at 790 K using the Redlich-Kwong equation of state:

$$P = \frac{RT}{V_m - b} - \frac{a}{\sqrt{T} V_m (V_m + b)} = \frac{nRT}{V - nb} - \frac{n^2 a}{\sqrt{T} V (V + nb)}$$

The Redlich-Kwong parameters  $a$  and  $b$  for benzene are  $452.0 \text{ bar dm}^6 \text{ mol}^{-2} \text{ K}^{1/2}$  and  $0.08271 \text{ dm}^3 \text{ mol}^{-1}$ , respectively. Is the attractive or repulsive portion of the potential dominant under these conditions?

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$$\begin{aligned}
 P &= \frac{RT}{V_m - b} - \frac{a}{\sqrt{T} V_m (V_m + b)} \\
 &= \frac{8.314 \times 10^{-2} \text{ bar dm}^3 \text{ mol}^{-1} \text{ K}^{-1} \times 790 \text{ K}}{1.42 \text{ dm}^3 \text{ mol}^{-1} - 0.08271 \text{ dm}^3 \text{ mol}^{-1}} \\
 &\quad - \frac{452.0 \text{ bar dm}^6 \text{ mol}^{-2} \text{ K}^{1/2}}{\sqrt{790 \text{ K}}} \times \frac{1}{1.42 \text{ dm}^3 \text{ mol}^{-1} \times (1.42 \text{ dm}^3 \text{ mol}^{-1} + 0.08271 \text{ dm}^3 \text{ mol}^{-1})}
 \end{aligned}$$

$$P = 41.6 \text{ bar}$$

$$P_{ideal} = \frac{RT}{V} = \frac{8.3145 \times 10^{-2} \times \text{L bar mol}^{-1} \text{ K}^{-1} \times 790 \text{ K}}{1.42 \text{ L}} = 46.3 \text{ bar}$$

Because  $P < P_{ideal}$ , the attractive part of the potential dominates.

**PROBLEM 2 (25 POINTS)**

1 mol of an ideal gas, for which  $C_{V,m} = 3/2R$ , initially at  $20.0^\circ\text{C}$  and  $1.00 \times 10^6 \text{ Pa}$  undergoes a two-stage transformation. For each of the stages described in the following list, calculate the final pressure, as well as  $q$ ,  $w$ ,  $\Delta U$ , and  $\Delta H$ . Also calculate  $q$ ,  $w$ ,  $\Delta U$ , and  $\Delta H$  for the complete process.

a) The gas is expanded isothermally and reversibly until the volume doubles.

b) Beginning at the end of the first stage, the temperature is raised to  $80.0^\circ\text{C}$  at constant volume.

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$$\text{a) } P_2 = \frac{P_1 V_1}{V_2} = \frac{P_1}{2} = 0.500 \times 10^6 \text{ Pa}$$

$$w = -nRT \ln \frac{V_2}{V_1} = -8.314 \text{ J mol}^{-1} \text{ K}^{-1} \times \ln 2 = -1.69 \times 10^3 \text{ J}$$

$$\Delta U = 0 \text{ and } \Delta H = 0 \text{ because } \Delta T = 0$$

$$q = -w = 1.69 \times 10^3 \text{ J}$$

$$\text{b) } \frac{T_1}{P_1} = \frac{T_2}{P_2}; P_2 = \frac{T_2 P_1}{T_1} = \frac{353 \text{ K} \times 0.500 \times 10^6 \text{ Pa}}{293 \text{ K}} = 6.02 \times 10^5 \text{ Pa}$$

$$\Delta U = nC_{V,m} \Delta T = 1.5 \times 8.314 \text{ J mol}^{-1} \text{ K}^{-1} \times (353 \text{ K} - 293 \text{ K}) = 748 \text{ J}$$

$$w = 0 \text{ because } \Delta V = 0$$

$$q = \Delta U = 748 \text{ J}$$

$$\begin{aligned} \Delta H &= nC_{P,m} \Delta T = n(C_{V,m} + R) \Delta T = \frac{3}{2} \times 8.314 \text{ J mol}^{-1} \text{ K}^{-1} \times (353 \text{ K} - 293 \text{ K}) \\ &= 1.25 \times 10^3 \text{ J} \end{aligned}$$

For the overall process,

$$q = 1.69 \times 10^3 \text{ J} + 748 \text{ J} = 2.44 \times 10^3 \text{ J}$$

$$w = -1.69 \times 10^3 \text{ J} + 0 = -1.69 \times 10^3 \text{ J}$$

$$\Delta U = 0 + 748 \text{ J} = 748 \text{ J}$$

$$\Delta H = 0 + 1.25 \times 10^3 \text{ J} = 1.25 \times 10^3 \text{ J}$$

**PROBLEM 3 (25 POINTS)**

Use the relation  $C_{P,m} - C_{V,m} = T \left( \frac{\partial V_m}{\partial T} \right)_P \left( \frac{\partial P}{\partial T} \right)_P$ , the cyclic rule, and the van der

Waals equation of state to derive an equation for  $C_{P,m} - C_{V,m}$  in terms of  $V_m$  and the gas constants  $R$ ,  $a$ , and  $b$ .

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We use the cyclic rule to evaluate  $\left( \frac{\partial V_m}{\partial T} \right)_P$ .

$$\left( \frac{\partial V_m}{\partial T} \right)_P \left( \frac{\partial T}{\partial P} \right)_{V_m} \left( \frac{\partial P}{\partial V_m} \right)_T = -1$$

$$\left( \frac{\partial V_m}{\partial T} \right)_P = - \left( \frac{\partial P}{\partial T} \right)_{V_m} \left( \frac{\partial V_m}{\partial P} \right)_T$$

$$C_{P,m} - C_{V,m} = T \left( \frac{\partial V_m}{\partial T} \right)_P \left( \frac{\partial P}{\partial T} \right)_{V_m} = -T \left[ \left( \frac{\partial P}{\partial T} \right)_{V_m} \right]^2 \left( \frac{\partial V_m}{\partial P} \right)_T = -T \frac{\left[ \left( \frac{\partial P}{\partial T} \right)_{V_m} \right]^2}{\left( \frac{\partial P}{\partial V_m} \right)_T}$$

$$P = \frac{RT}{V_m - b} - \frac{a}{V_m^2}$$

$$\left( \frac{\partial P}{\partial T} \right)_{V_m} = \frac{R}{V_m - b}$$

$$\left( \frac{\partial P}{\partial V_m} \right)_T = \frac{-RT}{(V_m - b)^2} + \frac{2a}{V_m^3} = \frac{-RTV_m^3 + 2a(V_m - b)}{V_m^3(V_m - b)^2}$$

$$C_{P,m} - C_{V,m} = -T \frac{\left( \frac{R}{V_m - b} \right)^2}{\frac{-RT}{(V_m - b)^2} + \frac{2a}{V_m^3}} = -T \frac{R}{-T + \frac{2a(V_m - b)^2}{RV_m^3}} = \frac{R}{1 - \frac{2a(V_m - b)^2}{RTV_m^3}}$$

In the ideal gas limit,  $a = 0$ , and  $C_{P,m} - C_{V,m} = R$ .

### PROBLEM 4 (25 POINTS)

Calculate the standard enthalpy of formation of  $\text{FeS}_2(s)$  at  $300^\circ\text{C}$  from the following data at  $25^\circ\text{C}$ . Assume that the heat capacities are independent of temperature. You are also given that for the reaction  $2\text{FeS}_2(s) + 11/2\text{O}_2(g) \rightarrow \text{Fe}_2\text{O}_3(s) + 4\text{SO}_2(g)$ ,  $\Delta H_{\text{reaction}}^\circ = -1655 \text{ kJ mol}^{-1}$ .

Substance	Fe(s)	FeS <sub>2</sub> (s)	Fe <sub>2</sub> O <sub>3</sub> (s)	S(rhombic)	SO <sub>2</sub> (g)
$\Delta H_f^\circ$ (kJ mol <sup>-1</sup> )			-824.2		-296.81
$C_{p,m}/R$	3.02	7.48		2.72	

$$\Delta H_{\text{reaction}}^\circ = \Delta H_f^\circ(\text{Fe}_2\text{O}_3, s) + 4\Delta H_f^\circ(\text{SO}_2, g) - 2\Delta H_f^\circ(\text{FeS}_2, s)$$

$$= -824.2 \text{ kJ mol}^{-1} - 1655 \text{ kJ mol}^{-1} - 1655 \text{ kJ mol}^{-1} - 1655 \text{ kJ mol}^{-1}$$

$$2\text{FeS}_2(s) + 11/2\text{O}_2(g) \rightarrow \text{Fe}_2\text{O}_3(s) + 4\text{SO}_2(g) \quad \Delta H_{\text{reaction}}^\circ = -1655 \text{ kJ mol}^{-1}$$

$$-1655 \text{ kJ mol}^{-1} = \Delta H_f^\circ(\text{Fe}_2\text{O}_3, s) + 4\Delta H_f^\circ(\text{SO}_2, g) - 2\Delta H_f^\circ(\text{FeS}_2, s)$$

$$\Delta H_f^\circ(\text{FeS}_2, s, 298 \text{ K}) = \frac{1655 \text{ kJ mol}^{-1} + \Delta H_f^\circ(\text{Fe}_2\text{O}_3, s) + 4\Delta H_f^\circ(\text{SO}_2, g)}{2}$$

$$= \frac{1655 - 824.2 - 4 \times 296.81 \text{ kJ mol}^{-1}}{2}$$

$$= -178.2 \text{ kJ mol}^{-1}$$

The enthalpy of formation at  $300^\circ\text{C}$  is given by

$$\Delta H_f^\circ(\text{FeS}_2(s), 573 \text{ K}) - \Delta H_f^\circ(\text{FeS}_2(s), 298 \text{ K}) + \int_{298 \text{ K}}^{573 \text{ K}} \Delta C_p(T) dT$$

Because the heat capacities are assumed to be independent of  $T$ ,

$$\Delta H_f^\circ(\text{FeS}_2(s), 573 \text{ K}) = \Delta H_f^\circ(\text{FeS}_2(s), 298 \text{ K})$$

$$+ [C_{p,m}(\text{FeS}_2, s) - C_{p,m}(\text{Fe}, s) - 2C_{p,m}(\text{S}, s)][573 \text{ K} - 298 \text{ K}]$$

$$= -178.2 \text{ kJ mol}^{-1} + 8.314 \text{ JK}^{-1} \text{ mol}^{-1} \times (7.48 - 3.02 - 2 \times 2.70) \times [573 \text{ K} - 298 \text{ K}]$$

$$= -180.0 \text{ kJ mol}^{-1}$$